

## 3/27 Lecture - Tritium Management

- 1) Side-stream
- 2) Units
- 3) Solubility in flibe
- 4) JUPITER II Paper

### 1) Side-stream

Concentration in flibe:  $C_T = (1.5) 10^{-5} \text{ g/m}^3$

↓  
Tritium inventory in flibe:  $M_T = (1.5) 10^{-3} \text{ g}$  ①

Tritium generation rate:  $Q_T = 95 \text{ g/yr} = (3) 10^{-6} \text{ g/s}$  ②

① + ②  $\Rightarrow$  Tritium residence time:  $\tau_T = \frac{M_T}{Q_T} = \boxed{500 \text{ sec.}}$

vs.

flibe inventory:  $M_{\text{flibe}} = 100 \text{ m}^3$  ③

flibe flow-rate:  $\dot{Q}_{\text{flibe}} = 2 \text{ m}^3/\text{s} = 3700 \text{ kg/s}$  ④

③ & ④  $\Rightarrow$   $\tau_{\text{flibe}} = \frac{M_{\text{flibe}}}{\dot{Q}_{\text{flibe}}} = \boxed{50 \text{ sec.}}$

Q: can we strip out tritium with a 5% side-stream?

in this case  $\tau_T / \tau_{\text{tube}} = 10 \Rightarrow$  tritium stripping can be achieved with a  $1/10$  side-stream.

explanation:

let  $x =$  side-stream fraction of primary coolant flow

$$x = \frac{\dot{Q}_{\text{strip}}}{\dot{Q}_{\text{tube}}}$$

stripping condition:  $Q_T \leq x \dot{Q}_{\text{tube}} C_T$

$$C_T = \frac{M_T}{M_{\text{tube}}} \Rightarrow x \geq \frac{Q_T}{M_T} \cdot \frac{M_{\text{tube}}}{\dot{Q}_{\text{tube}}} \Rightarrow$$

$$\Rightarrow \boxed{x \geq \frac{\tau_{\text{tube}}}{\tau_T}} \Rightarrow x \geq \frac{1}{10} \text{ in this case.}$$

2) units

$$30,000 \text{ Bi / mol T}$$

$$15,000 \text{ Bi / mol T}_2$$

$$\boxed{9600 \text{ Bi / g T}_2}$$

$\approx 10^4 \text{ Bi / g T}_2$

$$t_{1/2} = 12 \text{ yr} = (3.9) 10^8 \text{ s}$$

$$\lambda = \frac{\ln 2}{t_{1/2}} = (1.8) 10^{-9} \text{ 1/s}$$

$$\text{activity (Bi)} = \lambda N =$$

↑  
# atoms

$$PV = nRT$$

$$(101,000) \times = 1 \text{ R } (273 + 25)$$

$$= (8.3) \frac{\text{J}}{\text{K-mol}} \cdot 298$$

$$1 \text{ mol STP} = 22.4 \text{ m}^3 \Rightarrow 1 \text{ g T}_2 = 7.5 \text{ m}^3 \text{ STP}$$

0°C, 1 atm

$$1 \text{ g T} = 0.33 \text{ mol} = (6.02) 10^{23} (0.33) \text{ atoms}$$

$$(1.8) 10^{-9} (6.02) 10^{23} (0.33) = (3.5) 10^{14} \text{ Bq}$$

$$1 \text{ Bi} = (3.7) 10^{10} \text{ Bq} \Rightarrow 1 \text{ g T}_2 = 9600 \text{ Bi}$$

$$3 \text{ g / mol T}$$

$$6 \text{ g / mol T}_2$$

$$100 \text{ g/yr} = 10^8 \text{ Ci/yr} \approx 2,600 \text{ Ci/day} = 0.03 \text{ Ci/s}$$

$$1 \text{ yr} = 365 \text{ days} = (3.16) 10^7 \text{ sec.}$$

$$1 \text{ day} = (8.64) 10^4 \text{ sec.}$$

$$100 \text{ g/yr} = \frac{(100) 10^4 \text{ Ci}}{(3) 10^7 \text{ sec}} \approx 0.03 \text{ Ci/sec}$$

### 3) Mass Transport in the Salt

$D_{\text{pebble}} \approx 3 \mu\text{m}$

$A_{\text{pebbles}} \approx 2000 \text{ m}^2$

$$Q_T = (3) 10^{-6} \text{ g/s}$$

$$q_T'' = (1.5) 10^{-9} \text{ g/m}^2\text{-s}$$

Why  $C_T = 10^{-5} \text{ g/m}^3$  ?

for a pebble bed

Prandtl  $Pr = \frac{\nu}{\alpha}$  thermal diffusivity

Nusselt

$$Nu = 2 + 1.1 Re^{0.62} Pr^{0.33}$$

heat transfer

$$Sh = 2 + 1.1 Re^{0.62} Sc^{0.33}$$

mass transfer

Sherwood

$$Sh = \frac{h_{\text{mass}}}{D/L}$$

Schmidt  $Sc = \frac{\mu}{\rho D} = \frac{\nu}{D}$

$$Sc = \frac{\mu}{\rho D} = \frac{\nu}{D}$$

mass diffusivity

$$[D] = \text{m}^2/\text{s}$$

Time fibre:

$$D = (3.83) 10^{-9} \text{ m}^2/\text{s} \quad \left\{ \text{faster mass transport!} \right.$$

fibre

$$\alpha = (2.30) 10^{-7} \text{ m}^2/\text{s}$$

$$Sc \approx 900$$

$$Pr \approx 15$$

$$Sh \approx 500$$

$$Nu \approx 100$$

$$h_{\text{mass}} \approx (6.35) 10^{-5} \text{ m/s}$$

$$\Rightarrow C_T = \frac{(1.5) 10^{-9} \text{ g/m}^2\text{-s}}{(6.35) 10^{-5} \text{ m/s}} = (2) 10^{-5} \text{ g/m}^3$$

$$D/L = \frac{(3.83) 10^{-9}}{0.03} = (1.27) 10^{-7} \text{ m/s}$$

$$q_T'' = h_{\text{mass}} (C_T - C_{T,\text{surf}}) \quad \left\{ \begin{array}{l} \text{assume } 0 \\ \Rightarrow C_T = \frac{q_T''}{h_{\text{mass}}} \end{array} \right.$$

# Tritium diffusion through flibe Fukada (2005)

Ref 2-6 : Diff & Perm.

Ref 7: stagnant flibe

Ref 9: equ. 1

$$D = \frac{k_B T}{6\pi\mu r_a}$$

Stokes-Einstein Eqn.

$\mu$  = visc.

$r_a$  = molec diam. of diffusive species

$T$  = temp.

$$\frac{k_B}{6\pi} = \text{const} = \frac{(1.4) \cdot 10^{-23} \text{ J/K}}{6\pi} = (7.4) \cdot 10^{-25} \text{ J/K}$$

$\mu_{\text{flibe}} \approx 0.01 \text{ Pa-s}$  ( $r_a \approx 10 \text{ \AA} = 10^{-9} \text{ m}$ )  $\Rightarrow D \approx$

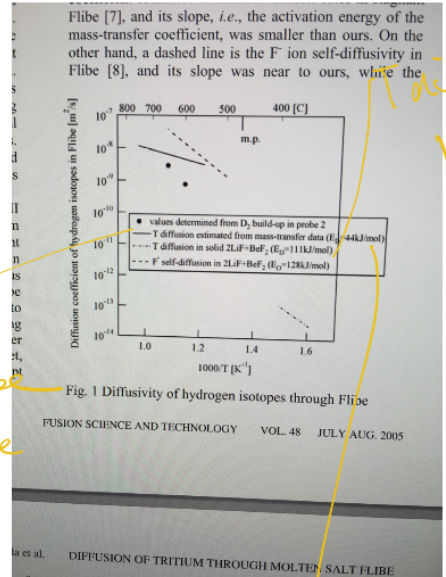
$$\text{slope} = \text{activation energy} = \left( \frac{k_B}{6\pi\mu r_a} \right)$$

$10^{-24}$   
 $(0.01) 10^{-9} \approx 10^{-15}$   
 $10^{-2}$   
 $10^{-11}$   
 $r_a = 10^{-5} \text{ m} = 10 \mu\text{m}$

- HF treated flibe
- dual-cylinder probe
- D2 down stream vs time vs upstream vs time

$h_{\text{mass}}$  in stagnant flibe

Ref 7.



diff @ low temp

Fig. 1 Diffusivity of hydrogen isotopes through Flibe  
FUSION SCIENCE AND TECHNOLOGY VOL. 48 JULY/AUG. 2005

la et al. DIFFUSION OF TRITIUM THROUGH MOLTEK-SALT FLIBE

# Jupiter II Paper

Ref 5

Tritium behavior in pipe depends on

- 1 chemical species → Ref 5
- 2 diffusivity of T<sup>+</sup> | Ref 6-10
- 3 solubility

Ref 11 }  
12 }  
15 }

Ref 13, 14

H<sub>2</sub> gas purge  $\xrightarrow[\text{exchange}]{\text{isotope}}$  HT  $\Rightarrow$  enhanced permeation through metal walls

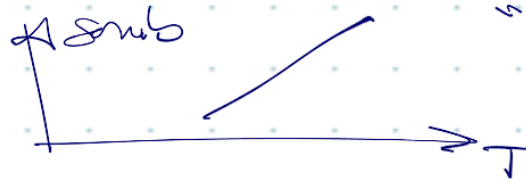
D<sub>2</sub>, H<sub>2</sub> solubility  $\approx \frac{1}{100}$  of HF, DF solub. @ 600°C

Reactive gases



↳ "Chemical  
Subst"

Inert gases



↳ "Physical  
Subst"

↳ "voids" or  
"holes" in  
structure of the  
molecular salt

$$-RT \ln \left( \frac{C_d}{C_g} \right) = KA S$$

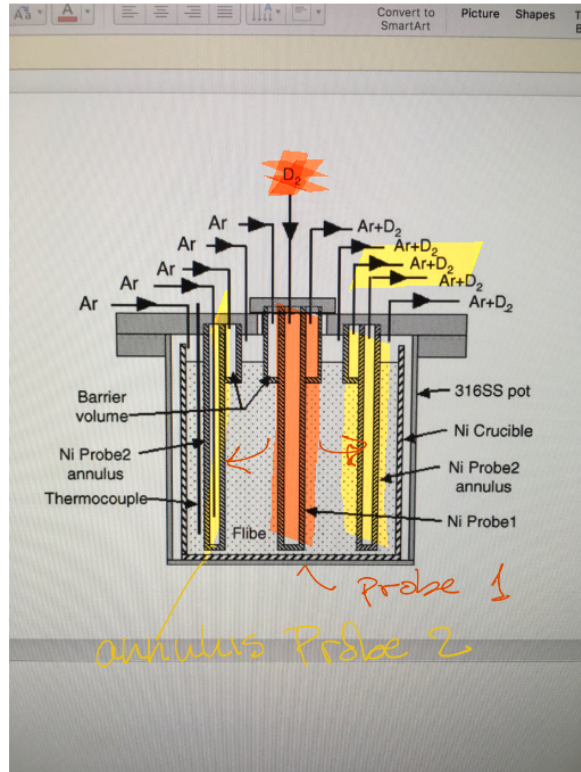
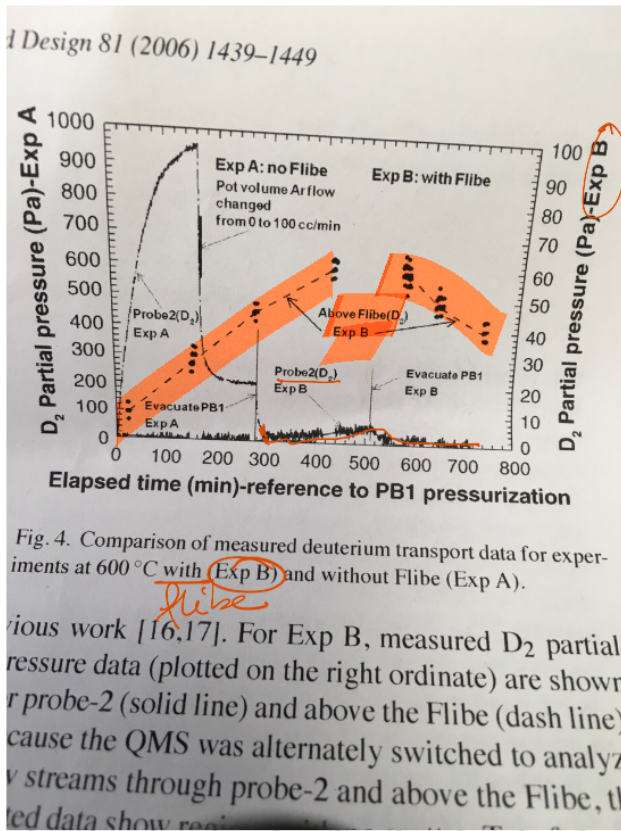
↳ total surf. area  
of holes

$$KA = 68.08 r^2$$

$r =$  atomic radius (Å)



# Jupiter Paper



- 1) Flibe-diffusion is rate-limiting, not Ni-permeation
- 2) Cover-gas  $P_2$  shows that salt-loading with  $D_2$  is happening while Probe 1 is filled w/ 90,000 Pa of  $D_2$ , then discharges once Probe 1 is flushed (i.e. source of  $D_2$  is removed).

@ 700 °C

$$K_c = (4) 10^{-3} \Rightarrow K_H = \frac{K_c}{RT} = (4) 10^{-3}$$

$$R = 8.3 \text{ J / K-mol}$$

$$T = 973 \text{ K}$$

$$\Rightarrow K_H = \frac{(4) 10^{-3}}{8076 \text{ J/mol}}$$

$$\Rightarrow K_H \approx (5) 10^{-7} \text{ mol / m}^3 \text{-Pa}$$

$$1 \text{ m}^3 = 1000 \text{ L}$$

$$\approx \frac{5(10)^{-7} \text{ mol}}{10^3 \text{ L} = 10^{-5} \text{ atm}} = (5) 10^{-5} \text{ mol/L atm}$$

$$c_T = (1.5) 10^{-5} \text{ g/m}^3 = (0.25) 10^{-5} \text{ mol T}_2/\text{m}^3$$

$$P_{T_2} = \frac{c_T}{K_H} = \frac{(0.25) 10^{-5} \text{ mol. / m}^3}{(5) 10^{-7} \text{ mol / m}^3 \text{-Pa}} = \boxed{5 \text{ Pa}}$$